



$$\left\{ \begin{array}{l} Pr < 1 \rightarrow \delta < \delta_T \\ Pr = 1 \rightarrow \delta = \delta_T \\ Pr > 1 \rightarrow \delta > \delta_T \end{array} \right. \quad \left( Pr = \frac{\nu}{\alpha} \right)$$

För gaser:  $\delta \approx \delta_T$  ( $Pr \approx 1$ )

## Gränsskiktanalys

$$Nu_x = \frac{h_x x}{k} = 0.332 Re_x^{\frac{1}{2}} Pr^{\frac{1}{3}} \quad (19-25)$$

$$Re_x = \frac{\rho v x}{\mu} = \frac{v x}{\nu}$$

medelvärde

$$Nu_L = 0.664 Re_L^{\frac{1}{2}} Pr^{\frac{1}{3}} = \frac{hL}{k} \quad (19-26)$$

$$Re_L = \frac{\rho v L}{\mu} = \frac{vL}{\nu}$$

## Gränsskikt för m-transport

$$\frac{C_{f,L}}{2} = 0.664 Re^{-\frac{1}{2}} = \frac{Nu_L}{Re_L Pr^{\frac{1}{3}}}$$

# Chilton - Colburn Analogin

$$j_H = j_D = \frac{C_f}{2}$$

$$j_H = \frac{Nu}{Re Pr^{\frac{1}{3}}}$$

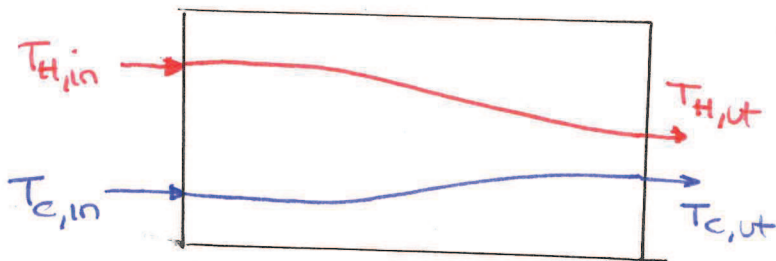
$$j_D = \frac{Nu_{AB}}{Re Sc^{\frac{1}{3}}}$$

Analogi: värme - värme - masstransport!

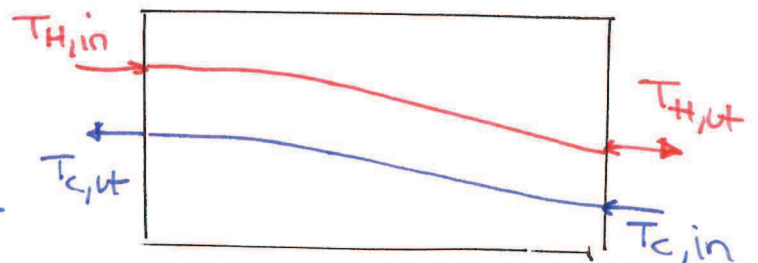
$Sc = \left\{ \text{Schmidt} \right\} = \frac{\nu}{D_{AB}}$  - diffusivitet av ett ämne

## Värmeväxlare

- Motström (counter-current-flow)
- Medström (co-current-flow)



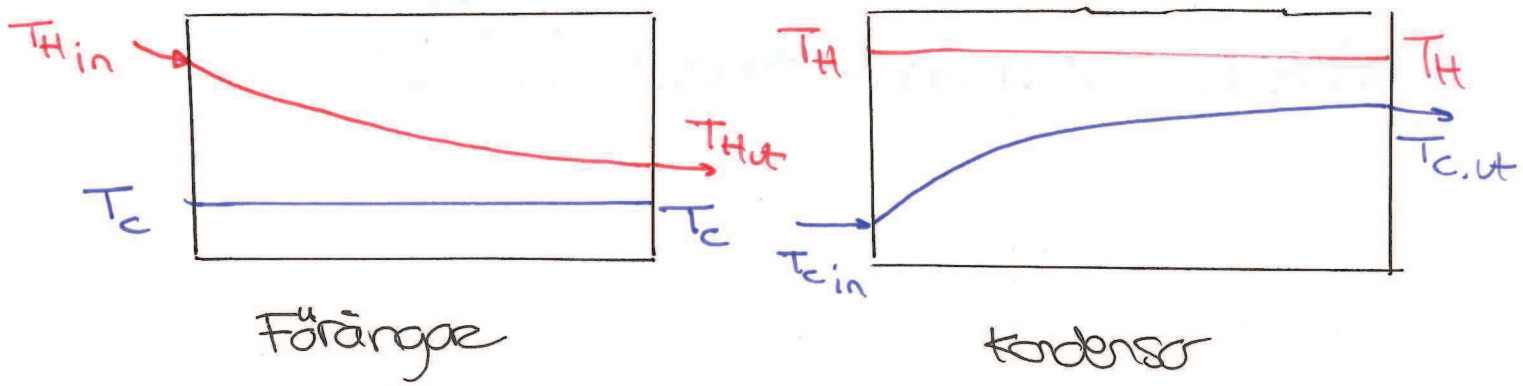
① Parallel flow



② counter flow

①  $T_{H,out} > T_{C,out}$

②  $T_{C,out}$  kan vara  $> T_{H,out}$



## Dimensionering av VVX

$$\dot{q} = UA \Delta T$$

$$\frac{1}{U_o A_o} = \frac{1}{A_i h_i} + \frac{\ln\left(\frac{r_o}{r_i}\right)}{2\pi k L} + \frac{1}{A_o h_o}$$

Fig 22.1

$\Delta T$ ? T-stillnad varmt/kallt

Logaritmskt medelvärde:  $\Delta T_{lm} = \frac{\Delta T_2 - \Delta T_1}{\ln\left(\frac{\Delta T_2}{\Delta T_1}\right)}$

Obs!  $\Delta T_{lm}$  gäller för både med- och motströms VVX

$$d\dot{q} = U dA (T_H - T_C) = (\dot{m} C_p)_C dT_C = (\dot{m} C_p)_H dT_H$$