

David Frisk **Demo 7**
KE-1

► Nu: Oljepanna, EO1, $\eta_p = 87\%$. Ånga 20ton/h, 10 bar, $200^\circ C$
Kondensat, $120^\circ C$, mättad

$$t_{drift} = 6500 \text{ h/år} \quad C_{EO1} = 271 \text{ kg/MWh bränsle}$$

► Efter: Kraftvärme, naturgas, $\eta_{tot} = 82\%$, $\alpha = 0.65 \frac{\text{MWh el}}{\text{MWh värme}}$
 $C_{NG} = 203 \text{ kg/MWh bränsle}$.

► Referensel kolkondens. $\eta_{el} = 92\%$, $\eta_{distr} = 96\%$.
 $C_{kol} = 327 \text{ kg/MWh bränsle}$.

$$Q_{ånga} = \dot{m}_{ånga} (h_{200^\circ C, 10 \text{ bar}} - h_{120^\circ C, \text{mättad}}) = \frac{20000}{3600} (2828 - 503,8) = 12,91 \text{ MW värme}$$

Pannan

$$C_{panna} = \frac{C_{EO1}}{\eta_{panna}} = \frac{271}{0,87} = 311 \text{ kg CO}_2/\text{MWh bränsle}$$

Kraftvärme

$$C_{onsite} = C_{NG} \left(\frac{1+\alpha}{\eta_+} \right) = 203 \left(\frac{1+0,65}{0,82} \right) =$$

Referensel

$$C_{offsite} = \frac{\alpha}{\eta_{distr} \eta_{el}} \cdot C_{kol}$$

$$\Rightarrow C_{CHP} = C_{onsite} - C_{offsite} = -119 \text{ kg CO}_2/\text{MWh värme}$$

$$\therefore \Delta C = C_{panna} - C_{CHP} = 311 - (-119) = 430 \text{ kg/mWh värme}$$

$$\Delta C_1 = \Delta C \cdot Q_{ånga} \cdot t_{drift} = 36,1 \text{ ton CO}_2/\text{år}$$